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Ultrasonic Behaviour of 1,1,2,2-Tetrachloroethane With An Alkane

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Experimental data for sound velocity and isentropic compressibility in binary mixtures of 1,1,2,2-tetrachloroethane with *n*-hexane, *n*-heptane, *n*-octane and *n*-nonane are reported at 303.15 and 313.15 K. Sound velocities have been analysed in terms of free length theory and collision factor theory. All the systems exhibited negative ΔK_s values.

1 INTRODUCTION

In continuation to our systematic study on excess thermodynamic properties and ultrasonic behaviour of binary mixtures of haloethane with a series of alkanes, alcohols and ketones,¹⁻⁹ we report here ultrasonic sound velocity and isentropic compressibility for the mixtures of 1,1,2,2-tetrachloroethane (hereafter referred to merely as TCE), with a series of *n*-alkanes at 303.15 and 313.15 K. The alkanes include *n*-hexane, *n*-heptane, *n*-octane and *n*-nonane. Sound velocity data have been analysed in terms of free length theory (FLT) of Jacobson,^{10,11}

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extended to binary mixtures by Kaulgud¹²⁻¹⁵ and collision factor theory (CFT) developed by Schaaffs^{16,17} extended to binary mixtures by Nutsch-Kuhnkeis¹⁸ to test their applicability to the present systems. The molar sound velocity¹⁹ (R), molar compressibility²⁰ (W), and van der Waals constant²¹ (b) which give information on molecular interactions have also been computed.

2 EXPERIMENTAL SECTION

TCE and *n*-alkanes were purified by the methods described earlier.⁹ The purity of the samples was checked by comparing the measured density of the samples with those reported in the literature.^{22,23} Isentropic compressibilities were calculated from precise densities and sound speed data determined at 303.15 and 313.15 K. Density was computed from measured excess volume data reported elsewhere,⁹ using the relation

$$\rho = \frac{x_1 M_1 + x_2 M_2}{V_m^i + V^E} \quad (1)$$

where x_i and M_i represent mole fraction and composition of component i respectively. V_m^i represents molar volume of ideal mixture and V^E is the excess volume. Ultrasonic sound velocity was measured with a single crystal interferometer²⁴ at a frequency of 2 MHz and was accurate to $\pm 0.1\%$ leading to an accuracy of $\pm 1 \text{ TPa}^{-1}$ in isentropic compressibility, K_s . All the measurements were made at a constant temperature employing a thermostat that could be maintained to $\pm 0.01 \text{ K}$.

3 RESULTS AND DISCUSSION

(a) Sound velocities

Theoretical aspects of FLT and CFT have been discussed in detail in earlier publications.^{2,4} Procedures for the calculation of R , W and b have also been described earlier.⁷ The surface area (Y) and collision factor (S) of the pure components used in FLT and CFT were calculated using the experimental sound velocity and density. Critical temperature, surface tension and the ratio of specific heats, which were used in the calculations of molar volume at absolute zero (V_0) and the average molecular radius (r_m), were taken from the literature.²²⁻²⁶ The values of molar volume (V_m), molar volume at absolute zero (V_0),

TABLE I
Values of V_m , V_0 , V_a , Y , S and r_m of the pure liquid components at 303.15 K

Component	V_m	V_0	V_a	L_f	Y	S	r_m
		cm ³ mol ⁻¹		A°			A°
1,1,2,2-tetrachloroethane	106.334	88.460	17.874	0.4433	80.645	1.4227	2.758
<i>n</i> -hexane	132.454	100.807	31.647	0.7429	85.199	1.4601	2.871
<i>n</i> -heptane	148.411	115.914	32.497	0.6918	93.948	1.4861	3.017
<i>n</i> -octane	164.478	130.889	33.589	0.6596	101.854	1.4951	3.151
<i>n</i> -nonane	180.755	145.943	34.812	0.6311	110.327	1.5132	3.275

TABLE II

Values of L_f^M , U exptl., U Theo (FLT), U Theo (CFT), $\Delta U\%$ (FLT) and $\Delta U\%$ (CFT), R , W and b for 1,1,2,2-tetrachloroethane with *n*-alkanes at 303.15 K

x_1	L_f^M A°	Exptl.	Theoretical			$\Delta U\%$ (FLT)	$\Delta U\%$ (CFT)	R	W	b cm ³ · mol ⁻¹
1	2	3	4	5	6	7	7	8	9	10
TCE + <i>n</i> -hexane										
0.0000	0.7429	1053	1053	1053	1053	0.00	0.00	1348	2441	238.9
0.1515	0.6978	1045	1032	1032	1063	1.24	1.77	1303	2418	234.8
0.2567	0.6661	1042	1026	1026	1071	1.58	2.81	1274	2399	231.9
0.3451	0.6395	1042	1025	1025	1077	1.71	3.46	1250	2383	229.6
0.4350	0.6123	1044	1027	1084	1084	1.64	3.93	1227	2366	227.1
0.6141	0.5580	1058	1044	1099	1099	1.34	3.92	1184	2333	222.3
0.7446	0.5190	1075	1065	1110	1110	0.92	3.28	1156	2308	218.7
0.8090	0.4998	1087	1079	1116	1116	0.75	2.65	1143	2300	217.0
0.9021	0.4722	1106	1103	1124	1124	0.32	1.63	1125	2285	214.5
1.0000	0.4433	1133	1133	1133	1133	0.00	0.00	1109	2271	211.8
Average % deviation										
						1.19	2.93			
TCE + <i>n</i> -heptane										
1	2	3	4	5	6	7	7	8	9	10
TCE + <i>n</i> -heptane										
0.0000	0.6918	1110	1110	1110	1110	0.00	0.00	1537	2791	227.2
0.1935	0.6516	1082	1078	1111	1111	0.38	2.66	1441	2688	264.6
0.3773	0.6095	1070	1063	1113	1113	0.63	4.04	1357	2669	252.5
0.4738	0.5889	1067	1062	1115	1115	0.48	4.51	1314	2539	246.2
0.5807	0.5587	1069	1065	1118	1118	0.37	4.55	1269	2483	239.2
0.6799	0.5329	1076	1072	1120	1120	0.35	4.13	1228	2431	232.7
0.7442	0.5154	1082	1080	1122	1122	0.18	3.74	1203	2397	228.5
0.8310	0.4914	1096	1094	1126	1126	0.22	2.71	1170	2354	222.9
0.8951	0.4732	1107	1107	1128	1128	0.01	1.93	1146	2322	218.7
1.0000	0.4433	1133	1133	1133	1133	0.00	0.00	1109	2271	211.8
Average % deviation										
						0.33	3.53			

TCE + <i>n</i> -octane									
1	2	3	4	5	6	7	8	9	10
0.0000	0.6596	1148	1148	1148	0.00	0.00	1722	3136	315.8
0.0000	0.6290	1116	1110	1141	0.53	2.23	1586	2962	294.9
0.2011	0.6095	1104	1097	1138	0.62	3.09	1518	2869	283.8
0.3081	0.5904	1096	1089	1136	0.68	3.64	1455	2782	273.5
0.4071	0.5692	1091	1084	1134	0.66	3.94	1392	2694	263.0
0.5082	0.5347	1092	1087	1132	0.46	3.65	1277	2527	243.0
0.7005	0.5041	1097	1094	1131	0.29	3.15	1220	2456	234.5
0.7816	0.4866	1104	1102	1131	0.19	2.49	1192	2399	227.6
0.8478	0.4696	1113	1112	1132	0.07	1.70	1157	2347	221.2
0.9096	0.4433	1133	1133	1133	0.00	0.00	1109	2271	211.8
1.0000									
Average % deviation									
				0.44	2.99				
• TCE + <i>n</i> -nonane									
1	2	3	4	5	6	7	8	9	10
0.0000	0.6311	1187	1187	1187	0.00	0.00	1914	3490	354.6
0.1853	0.6103	1153	1149	1174	0.40	1.81	1754	3262	328.2
0.3160	0.5919	1134	1128	1166	0.52	2.77	1644	3104	309.5
0.4111	0.5767	1123	1117	1160	0.55	3.27	1565	2956	295.9
0.5334	0.5534	1112	1108	1152	0.45	3.65	1461	2849	277.5
0.5396	0.5191	1106	1104	1144	0.20	3.47	1331	2599	254.1
0.7035	0.4965	1107	1108	1140	0.09	3.00	1256	2516	240.3
0.8900	0.4839	1111	1112	1138	0.09	2.39	1219	2433	233.2
0.8502	0.4670	1116	1118	1135	0.24	1.76	1170	2368	223.9
0.9153	0.4433	1133	1133	1133	0.00	0.00	1109	2271	211.8
1.0000									
Average % deviation									
				0.36	2.77				

TABLE III

Volume fraction ϕ_1 , of 1,1,2,2-tetrachloroethane, density ρ , speed of sound U , isentropic compressibility K_s , calculated from Eq. 2 and K_s calculated from Eq. 3, for 1,1,2,2-tetrachloroethane + *n*-alkanes at 303.15 and 313.15 K.

ϕ_1	$\rho/\text{g cm}^{-3}$	U/ms^{-1}	K_s/TPa^{-1}	$\Delta K_s/\text{TPa}^{-1}$	ϕ_1	$\rho/\text{g cm}^{-3}$	U/ms^{-1}	K_s/TPa^{-1}	$\Delta K_s/\text{TPa}^{-1}$
1	2	3	4	5	6	7	8	9	10
303.15 K									
TCE + <i>n</i> -hexane									
0.0000	0.65064	1053	1386	0	0.0000	0.64058	1012	1524	0
0.1254	0.76742	1045	1193	-81	0.1381	0.76933	995	1313	-73
0.2171	0.85291	1042	1080	-112	0.2296	0.85459	992	1189	-106
0.2973	0.92764	1042	993	-128	0.2790	0.90064	993	1126	-120
0.3820	1.00656	1044	911	-134	0.3737	0.98868	998	1016	-135
0.5609	1.17312	1058	762	-124	0.4634	1.07194	1006	922	-140
0.7006	1.30262	1075	664	-97	0.5959	1.19464	1024	798	-131
0.7727	1.36931	1087	618	-79	0.7088	1.29870	1044	706	-110
0.8809	1.46906	1106	556	-44	0.7771	1.36161	1057	657	-91
1.0000	1.57851	1133	494	0	1.0000	1.56619	1102	526	0
TCE + <i>n</i> -heptane									
1	2	3	4	5	6	7	8	9	10
0.0000	0.67522	1110	1202	0	0.0000	0.66678	1070	1310	0
0.1467	0.80713	1082	1058	-40	0.1244	0.73716	1044	1179	-33
0.2672	0.91577	1070	954	-59	0.2239	0.77821	1032	1082	-52
0.3921	1.02859	1067	854	-70	0.2874	0.92477	1028	1023	-62
0.4981	1.12437	1069	778	-71	0.3663	0.99577	1029	948	-75
0.6035	1.21965	1076	708	-67	0.4562	1.07674	1032	872	-80
0.6758	1.28519	1082	665	-59	0.5977	1.20433	1044	766	-75
0.7789	1.37854	1096	604	-47	0.6974	1.29413	1049	702	-61
0.8594	1.45151	1107	562	-32	0.8545	1.43557	1071	607	-33
1.0000	1.57851	1133	494	0	1.0000	1.56619	1102	526	0

		TCE + <i>n</i> -octane			
0.0000	0.67450	1093	0	0.68639	1108
0.1400	0.81684	1116	983	0.81546	1074
0.2235	0.89028	1104	922	0.88530	1064
0.3074	0.96404	1096	864	0.92830	1058
0.4005	1.04609	1091	803	1.05100	1052
0.6019	1.22428	1092	685	1.12378	1052
0.6982	1.30966	1097	635	1.21268	1055
0.7827	1.38468	1104	593	1.30893	1062
0.8668	1.45955	1113	553	1.42870	1076
1.0000	1.57851	1133	494	1.56619	1102
			0	0	0
		TCE + <i>n</i> -nonane			
0.0000	0.70958	1187	1000	0	0.70212
0.1181	0.81092	1153	930	-12	0.81919
0.2138	0.89320	1134	871	-21	0.89688
0.2912	0.95999	1123	826	-27	0.92474
0.4082	1.06127	1112	762	-31	1.05804
0.5827	1.21302	1106	674	-31	1.12181
0.7019	1.31703	1107	616	-25	1.19777
0.7696	1.37630	1111	591	-22	1.32806
0.8641	1.45908	1116	550	-13	1.36128
1.0000	1.57851	1133	494	0	1.56619
			0	0	0

available volume (V_a), free length (L_f), surface area (Y), collision factor (S) and the average radius of the molecules (r_m) of the pure components are given in Table I. The free lengths of the binary mixtures and sound velocity data predicted in terms of FLT and CFT are given in Table II along with experimental results in columns 2 to 5. The percentage deviation between the experimental sound velocity data and those of the FLT and CFT values are given in columns 6 and 7 along with average percentage deviation. Values of R , W and b are also given in columns 8-10 of Table II.

The results given in columns 3-7 of Table II reveal that the FLT sound velocities are in excellent agreement with the experimental results in all the systems. The maximum average percentage deviation in any system does not exceed 0.44% (except in case of *n*-hexane). The maximum individual deviation is 1.71%. However, the sound velocities estimated by CFT are not in good agreement with the experimental results. The average percentage deviation varies from 2.77 to 3.53. The maximum individual deviation in case of CFT is 4.55%. Venkateswarlu *et al.*²⁷ have also reported similar observations in their recent publication.

The data included in columns 8 to 10 of Table II show that the values of R , W and b exhibit linear relationship with mole fraction in all the systems studied as expected. This in turn shows the absence of strong interactions between unlike molecules.

(b) Isentropic compressibility

Isentropic compressibility (K_s) was calculated using the relation

$$K_s = U^{-2} \rho^{-1} \quad (2)$$

where U and ρ denote the sound velocity and density. The deviation in K_s from ideal behaviour, assumed to be additive in terms of volume fraction, is estimated using the equation

$$\Delta K_s = K_s - \phi K_{s1} - (1 - \phi) K_{s2} \quad (3)$$

where K_{s1} and K_{s2} are the isentropic compressibilities of the pure components 1 and 2 respectively. ϕ is the volume fraction of TCE.

Experimental data for ρ , U , K_s and ΔK_s at 303.15 and 313.15 K are included in Table III. The dependence of ΔK_s on volume fraction is expressed by an empirical equation of the form

$$\Delta K_s = \phi(1 - k) \left\{ \sum_{j=0}^{n-1} b_j (1 - 2\phi)^j \right\} \quad (4)$$

TABLE IV

Standard deviation $\sigma (\Delta K_s)$ and values of parameters b_j for the systems of TCE + *n*-alkanes at 303.15 and 313.15 K

System	b_0	b_1	b_2	b_3	$\sigma(\Delta K_s)/\text{TPa}^{-1}$
Temp. 303.15 K					
TCE + <i>n</i> -hexane	-521.0	166.9	-103.6	78.1	0.6
TCE + <i>n</i> -heptane	-284.0	36.1	-16.8	—	0.7
TCE + <i>n</i> -octane	-201.8	30.7	7.2	-13.5	0.3
TCE + <i>n</i> -nonane	-130.1	4.9	28.2	—	0.7
Temp. 313.15 K					
TCE + <i>n</i> -hexane	-558.0	76.5	-19.7	-27.1	0.4
TCE + <i>n</i> -heptane	-315.0	23.8	66.7	—	1.7
TCE + <i>n</i> -octane	-210.4	11.1	39.1	23.8	0.5
TCE + <i>n</i> -nonane	-134.9	-0.4	64.9	—	0.9

The values of b_j calculated by the method of least squares are given in Table IV along with the standard deviation $\sigma (\Delta K_s)$.

The results included in Table III show that ΔK_s is negative over the whole range of composition in all the mixtures at both the temperatures. Such an observation is not common in nonpolar systems. The negative values of ΔK_s for the four systems fall in the order: *n*-hexane > *n*-heptane > *n*-octane > *n*-nonane. The temperature coefficient of ΔK_s is negative in all the systems.

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